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Humidity calibration equipment for food processing applications

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Humidity measurements at high temperatures and under non-static conditions, PTB, Braunschweig, Germany 16 to 17 November 2017

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Background and motivations





- Drying is estimated to cost EU industry some 30 billion € per year in energy costs. Every 0.1 % improvement in drying efficiency due to better process control could save around 30 M€/year.
- Monitoring humidity at temperatures above 100 °C is a key factor in controlling drying processes.
- The **food industry** is the second largest manufacturing sector in the EU with a total manufacturing turnover of over 900 billion Euto.
- Drying and baking are key processes in the food industry and humidity control is a key parameter in controlling product quality.

Environment motivations



- The European Directive 2012/27/EU on **Energy Efficiency** and the identification of improving energy efficiency as one of the most effective way to reduce **greenhouse emissions** and other pollutants and thus to **mitigate climate change.**
- The reliability of humidity measurements directly affects the drying efficiency, and significant savings are expected by the outcomes of this project.
- The targeted improvements in energy efficiency through better humidity monitoring in drying processes would result in



Significant reduction in the **emissions**



Improvements in process control



Reduce **waste** material



Industrial demand



Although humidity measurements are carried out in many processes **significantly above 100** °C and humidity sensors are specified for such conditions, humidity **calibrations are usually not performed at temperatures above 100** °C and the calibration equipments available in the industry cannot be operated in this range.



Example of tunnel oven-drying and roasting: 45-50 minutes at **140** °C for a mild processing to ensure a good final quality in terms of residual water content (<1%), lipid oxidation and color. Alternatively, nuts are heated up to **180** °C for 20 minutes in fast drying process.

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Design criteria



To support the **operating range of industrial dryers**, the generator :

- is based on controlled, SI-traceable, mixing of a water mass flow evaporated into a dry air mass flow
- air temperature up to 180 °C
- dew-point temperature up to 140 °C
- pressure up to 6 bar(abs)



 The vapor/steam generator should operate over a wide range of absolute humidity, from 25 g/m³ at atmospheric pressure to 1000 g/m³ at 6 bar(abs).





Working principle





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Experimental set up I







XIII International Symposium on Temperature and Thermal Measurements in Industry and Science – Zakopane-2016

Experimental set up II





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QSR hygrometry I



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QSR hygrometry II





experimentally, to determine \mathcal{E}_{Mix} using a mw resonator resonance frequencies f(and half-widths g) are, for instance, measured at the same temperature T in vacuum and at pressure p

$$\varepsilon_{\rm mix} = \left(\frac{\langle f+g\rangle_0}{\langle f+g\rangle_p}\right)^2 = \left(\frac{\langle f+g\rangle_0}{\langle f+g\rangle_p \left(1-k_T p/3\right)}\right)^2$$

and the isothermal compressibility of the cavity k_T can be determined from measurements in He as a function of pressure

Pressure control





Initial design

Sensor and actuator were far from each other Stability of pressure is about **4 per thousand** P is source of 70% of the uncertainty Forming of droplets inside the cold trap is a source of instability Sensor and actuator are side by side -> no delay Stability of pressure is about **1 per thousand** Cascade control of pressure by using two different control units. Significant reduction of the uncertainty

revised design

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Results I – response time





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Uncertainty evaluation





the uncertainty in the independent knowledge of the polarizability of water (Debye constants) dominates

	Reference date	A	В
Groves and Sugden	1935	4.3 ± 1.2	(2.074±0.054)×104
Stranathan	1935	4.03 ± 0.39	$(2.071 \pm 0.014) \times 10^{4}$
Hurdes and Smyth	1942	3.4 ± 1.2	$(2.087 \pm 0.053) \times 10^{4}$
Essen and Froome	1951	3.585 ± 0.011	$(2.061 \pm 0.002) \times 10^4$
Birnbaum and Chatterjee	1952	3.84 ± 0.72	$(2.092 \pm 0.024) \times 10^{4}$
Essen	1953	4.157 ± 0.012	$(2.041 \pm 0.002) \times 10^{4}$
Boudouris	1958	3.99 ±0.60	$(2.081 \pm 0.020) \times 10^{4}$

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QSR vs. CMH calculation





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QSR vs. Mass flow calculation





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Operating range





- The operating range is defined <u>above</u> the plot surface.
- Generator has been validated against traceable CMH and QSR hygrometers at 55 different points.
- Tests has been carried out with nitrogen and air.

	Min	Max
Temperature [°C]	60	161
Pressure [bar]	1.02	6.08
Specific Humidity [kg/kg]	0.07	0.646
Dew Point Temperature [°C]	38	142.44
Flow [l/m]	1	40

Validation over the operating orange





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Conclusions



- A mass fraction humidity generator has been developed at INRIM to provide traceable calibrations of humidity sensors at temperatures above 100 °C.
- The principle of operation is based on mixing and evaporating a known mass of water into a known mass of dry air.
- The generator operates up to 180 °C, with dew point temperatures up to 140 °C and pressures up to 6 bar(abs).
- A gold-plated quasi-spherical microwave resonator (QRS) has been integrated with a mass fraction humidity generator developed at INRIM.
- The humidity generator has been thoroughly validated at 55 different operation conditions against CMH and QSR.



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